

## Oxidative Dehydrogenation of Ethane over MoVTeNbO Catalyst Prepared by a Slurry Method

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The oxidative dehydrogenation (ODH) of ethane to ethene has attracted much attention in recent years. López Nieto *et al.*<sup>[1]</sup> reported that MoVTeNbO catalysts prepared by hydrothermal synthesis show high activity and selectivity for ODH of ethane, and an ethene yield of 75 % was obtained at 400 °C on the best catalysts. In ethane oxidation, the catalytic behavior of MoVTeNbO catalysts can be mainly related to the presence of the multifunctional  $\text{Te}_2\text{M}_{20}\text{O}_{57}$  orthorhombic phase in cooperation with the (V,Nb)-containing  $\text{Mo}_5\text{O}_{14}$ -type phase<sup>[2,3]</sup>.

In this paper, we report the preparation of the MoVTeNbO catalyst by a slurry method, its characterization and the influence of the calcination atmosphere on the catalyst performance for the ODH of ethane.

The MoVTeNbO catalyst was prepared by a slurry method. Ammonium heptamolybdate, ammonium metavanadate and telluric acid were dissolved upon heating to 80 °C in a flask, and niobium oxalate was dissolved in another flask. The atomic ratio of Mo V Te Nb was 1 0.3 0.23 0.1. The aqueous solution of niobium oxalate was added to the first flask to result in a slurry. The water in this slurry was removed by a rotary evaporator to obtain the precursor solid. After it was dried at 80 °C for 10 h, the precursor solid was calcined at 600 °C for 2 h in a  $\text{N}_2$  stream (the sample is denoted as SL-N). For comparison, the same precursor solid was calcined at 600 °C for 2 h in air (denoted as SL-A).

The catalytic performance of the MoVTeNbO catalyst for the ODH of ethane was tested in a fixed-bed quartz tubular reactor at atmospheric pressure. The result is shown in Table 1. SL-N showed good catalytic performance for the ODH of ethane to ethene at reaction temperatures above 400 °C, and ethene was formed as the main product. The ethane conversion increased and the selectivity for ethene decreased with increasing temperature. A maximum ethene yield of 80.9 % was achieved at 440 °C on SL-N. However, on SL-A almost no activity for the ODH of ethane was detected.

Table 1 ODH of ethane on MoVTeNbO catalyst samples

Sample	<i>t</i> / °C	<i>X</i> / %	<i>S</i> / %			<i>Y</i> / %
			$\text{C}_2\text{H}_4$	CO	$\text{CO}_2$	
Blank	440	—	—	—	—	—
SL-N	400	59.0	95.4	0.8	3.8	56.3
	420	75.5	93.6	1.4	5.0	70.7
	440	89.6	90.3	1.5	8.2	80.9
	460	95.8	83.4	3.9	12.8	79.9
SL-A	440	—	—	—	—	—

Reaction conditions: 500 mg catalyst, total flow rate 10 ml/min, feed composition 30 %  $\text{C}_2\text{H}_6$ -30 %  $\text{O}_2$ -40 %  $\text{N}_2$ .

XRD patterns of the MoVTeNbO catalyst are shown in Fig 1. SL-A was primarily composed of the  $\text{MoO}_3$  phase but no  $\text{MoO}_3$  was observed in the pattern of SL-N. SL-N gave peaks at  $2\theta = 7.7^\circ, 9.0^\circ, 22.1^\circ, 26.2^\circ, 26.8^\circ, 27.3^\circ, 29.2^\circ$  and  $35.4^\circ$ , which were mainly related to an orthorhombic  $\text{Te}_2\text{M}_{20}\text{O}_{57}$  (M = Mo, V and Nb) phase, while peaks

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at  $7.7^\circ$ ,  $8.7^\circ$ ,  $14.0^\circ$ ,  $22.1^\circ$ ,  $23.3^\circ$ ,  $24.9^\circ$ ,  $29.7^\circ$ ,  $31.5^\circ$ ,  $32.4^\circ$  and  $33.5^\circ$  were attributed to  $(\text{Mo}_{0.93}\text{V}_{0.07})_5\text{O}_{14}$  [JCPDS, 31-1437] and/or  $\text{Nb}_{0.09}\text{Mo}_{0.91}\text{O}_{2.80}$  [JCPDS, 27-1310] or  $\text{Mo}_{5-x}(\text{V}/\text{Nb})_x\text{O}_{14}$ -like phases. The peaks at  $22.1^\circ$ ,  $28.2^\circ$ ,  $36.2^\circ$ ,  $45.2^\circ$  and  $50.0^\circ$  were assigned to the  $\text{Te}_{0.33}\text{MO}_3$  ( $\text{M} = \text{Mo}$ ,  $\text{V}$ , and  $\text{Nb}$ ) phase<sup>[2~4]</sup>.

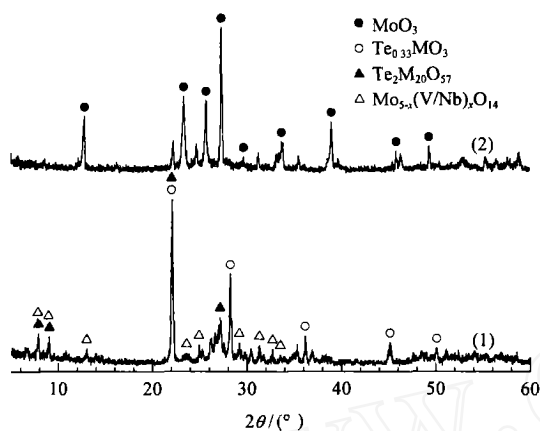


Fig 1 XRD patterns of solid MoVTeNbO catalyst samples  
(1) SL-N, (2) SL-A

The difference in the surface morphology of the two samples was revealed by SEM, as shown in Fig 2. SL-A has plate-like structure with fairly smooth surfaces, while SL-N has a porous surface morphology with some fine structure, which was in good agreement with the surface area measurements. The BET specific surface area of SL-N was  $6.92 \text{ m}^2/\text{g}$ , while that of SL-A was only  $0.31 \text{ m}^2/\text{g}$ . This result also agreed with the finding by Watanabe *et al*<sup>[5]</sup> that a higher surface area of the catalyst correlated well with a higher catalytic activity.

In conclusion, the MoVTeNbO catalyst prepared by the slurry method and calcined at  $600^\circ\text{C}$  in a  $\text{N}_2$  stream exhibits an ethane conversion of 90 % and an ethene selectivity of 90 % at  $440^\circ\text{C}$ . A highly crys-

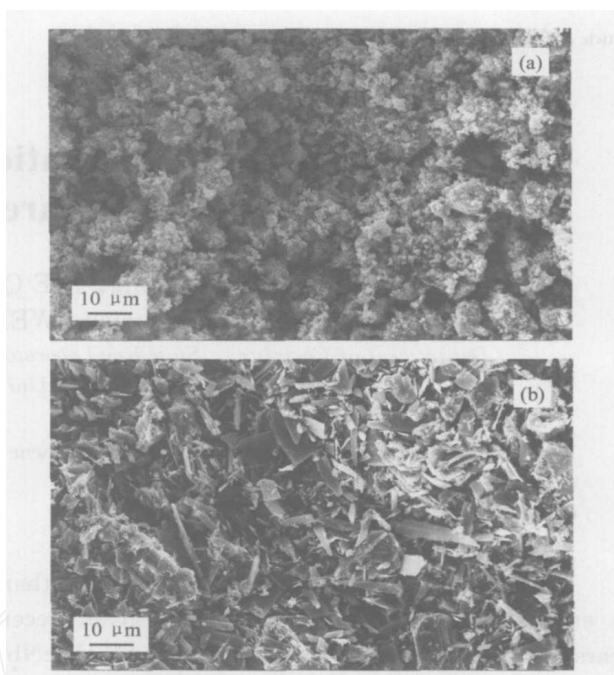


Fig 2 SEM images of MoVTeNbO catalyst samples  
(a) SL-N, (b) SL-A

talline MoVTeNbO catalyst may be one of the most effective catalysts for ethene production using low cost ethane.

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## 浆态法制备的 MoVTeNbO 催化剂上的乙烷氧化脱氢

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摘要: 采用浆态法在  $\text{N}_2$  气氛下焙烧制得了  $\text{MoV}_{0.3}\text{Te}_{0.23}\text{Nb}_{0.1}\text{O}_x$  催化剂。在以该催化剂催化的乙烷氧化脱氢制乙烯的反应中,  $440^\circ\text{C}$  下乙烷的转化率和乙烯的选择性均在 90 % 左右, 乙烯产率达 80.9 %。但在空气气氛下焙烧得到的催化剂几乎没有催化活性。用 XRD 和 SEM 等方法考察了催化剂的结构。

关键词: 乙烷, 氧化脱氢, 乙烯, 氧化钼, 氧化钽, 氧化铌, 混合金属氧化物催化剂

(Ed L YX)